

# Modeling a Concentrated Solar Thermal Collector for Methane Dry Reforming

## Introduction

There are tremendous research efforts focused on capturing thermal energy from the sun. Our current application is using this heat to drive a chemical reaction called dry reforming that produces hydrogen from methane and carbon dioxide, 2 potent greenhouse gases. This reaction only occurs at high temperatures, requiring concentrated solar power.

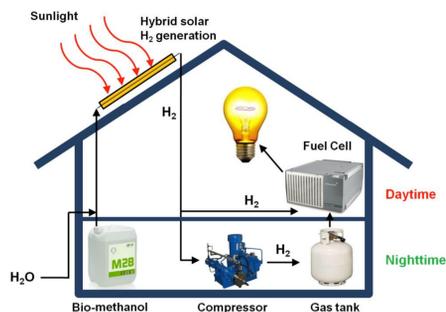


Figure 1. Schematic of overall residential hydrogen production system

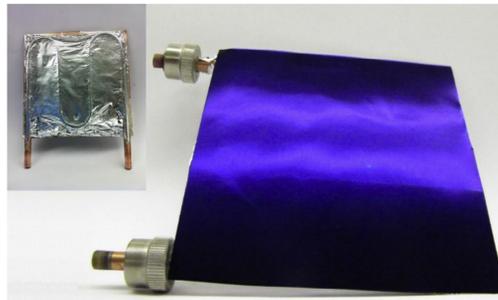


Figure 2. Solar thermal absorber placed inside a vacuum-insulated collector

Modeling the operation of a concentrated solar collector is complex as the physics are highly coupled. Fluid flow of 50% mole fraction CH<sub>4</sub> and CO<sub>2</sub> is introduced at the inlet. The fluid is then heated through contact with a solar absorber, then reacted by flowing through a packed catalyst bed to form H<sub>2</sub> and CO. The following multiphysics model describes the operation of a collector, investigating the influence of various parameters on overall efficiency and H<sub>2</sub> generation.

## Computational Methods

Since the problem includes heat transfer, fluid dynamics, and reaction, the physics interfaces used were Heat Transfer, Laminar Flow, Transport of Concentrated Species, and Chemistry. Non-isothermal and Reacting Flow multiphysics were used to properly couple the various physics.

Within the Heat Transfer physics, surface-to-surface radiation was considered. This was important to define the optical properties of the absorption coating and emissivity of other surfaces. Participating media was initially considered, but it had negligible effects due to the low absorption coefficient of the gases in question.

The equations used are listed below:

$$\text{Heat Transfer } \rho c_p \mathbf{u} \cdot \nabla T + \nabla \cdot \mathbf{q} = Q \quad \mathbf{q} = -k \nabla T$$

$$\text{Laminar Flow } \rho(\mathbf{u} \cdot \nabla) \mathbf{u} = \nabla \cdot \left[ -p \mathbf{I} + \mu (\nabla \mathbf{u} + (\nabla \mathbf{u})^T) - \frac{2}{3} \mu (\nabla \cdot \mathbf{u}) \mathbf{I} \right] + \mathbf{F}$$

$$\nabla \cdot (\rho \mathbf{u}) = 0$$

$$\text{Reacting Flow } \nabla \cdot \mathbf{j}_i + \rho(\mathbf{u} \cdot \nabla) \omega_i = R_i \quad \mathbf{N}_i = \mathbf{j}_i + \rho \omega_i$$

$$R_i = \nu_i \left[ A^f \exp \left( \frac{-E^f}{R_0 T} \right) \right] \prod_{i=1}^{Q_r} c_i^{\nu_i}$$

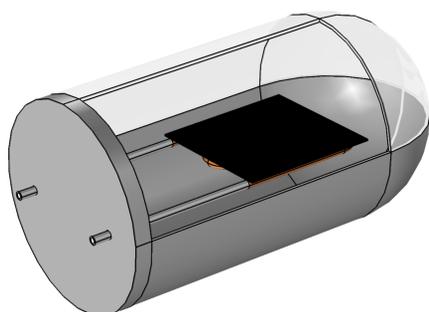


Figure 3. Geometry of overall 3D model including glass cover and steel bulkhead

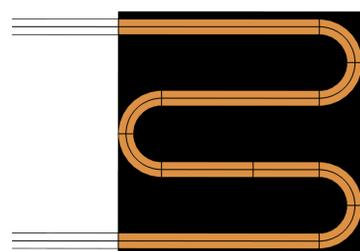


Figure 4. Geometry of copper tube layout underneath absorption coating

## Results

### Materials Analysis

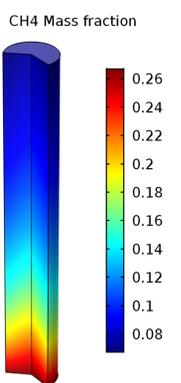
Copper tubes have been used in the past due to their high thermal conductivity. However, this results in high losses, especially considering the thermal short circuit created by the looped entry-exit. Therefore, various other better-insulating materials were modeled.

Material	Thermal Cond (W/mK)	Coating Temp (K)
Copper	400	971.9
Aluminum	238	988.9
Steel	44.5	1011.2
Alumina	27.0	1013.4
Silica Glass	1.38	1017.1

### Catalytic Reaction Tuning

Instead of modeling a porous media for the packed catalyst bed, a simple control volume reactor was used. To tune the reaction, the activation energy and pre-exponential constant were varied to accurately match experimental data. The final values were:

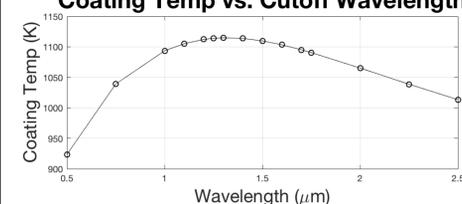
$$E_f = 90 \frac{\text{kJ}}{\text{mol}}, \quad A_f = 5e5 \frac{\text{m}^3}{\text{mol s}}$$



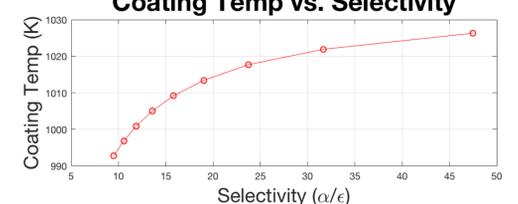
### Absorption Coating Properties

The optical properties of the absorption coating are critical to operation. High-temperature selective absorbers are difficult to make, so their properties should be determined before fabrication. The model was run for various cutoff wavelengths and selectivities to maximize temperature.

#### Coating Temp vs. Cutoff Wavelength

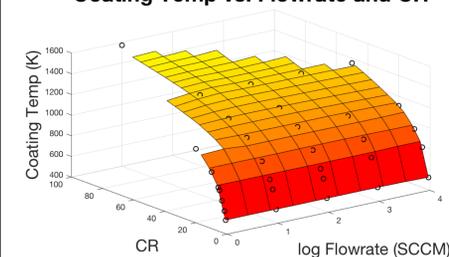


#### Coating Temp vs. Selectivity

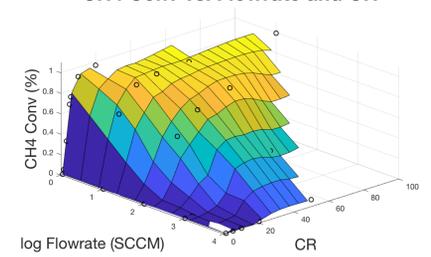


### Steady State Results

#### Coating Temp vs. Flowrate and CR



#### CH4 Conv. vs. Flowrate and CR



## Conclusions

- Numerical model was successfully created to determine conversion and efficiency for various flowrates and concentration ratios
- Results show concentrated solar thermal power is effective in producing hydrogen from methane
- Optical properties of the absorption must be tuned properly to optimize efficiency and create the ideal collector
- Future work in fabricating a high-temperature coating

## REFERENCES

- Real et al. "Novel non-concentrating solar collector for intermediate-temperature energy capture" Solar Energy 108 (2014). Duke University.