Modeling of a Multilayered Propellant Extrusion in Concentric Cylinders S. Durand¹⁻³, C. Dubois¹, P. Lafleur¹, V. Panchal², D. Park², D. Lepage³, P.Y. Paradis³ 1. École Polytechnique de Montréal, T [} d.æ #Ű Ô ÉÔæ) æåæ 2. US Army ARDEC, Picatinny Arsenal, NJÉNÙŒ 3. General Dynamics Ordnance and Tactical Systems – Canada, Valleyfield, QÔ, Canada

Introduction: This work was focused to demonstrate the effects of an extrusion die design on the flow balance between two unconnected layers, a highly viscous material separated by an inner layer of a more liquidlike material. The two viscous layers come from the same pressure driven flow but use warmer different path lengths throughout the die.

The propellant dough being a thermal poor conductor, the section inner becomes

▲ 3.8489×10⁻³ 0.0035 0.003 0.0025 0.002 0.0015



Figure 1. Multilayered propellant grain

Computational Methods: Using COMSOL CFD and Heat Transfer modules, a study has been conducted

than the middle and section outer due to viscous heating.



Figure 3. Velocity profile



multiple die on 294 configurations to find an 293.5 optimized design that ▼ 293.15 enables extrusion process Figure 2. Cross section of die Figure 4. Temperature distribution within flow model of wide range od viscoelastic materials with different rheological
Table 1. Simulation data
 properties while maintaining the flow model balanced. The viscosity as a function of temperature was expressed with the Arrhenius equation as follow:

$$\eta(\dot{\gamma}, T) = \eta_0 \exp\left[\frac{E}{R} * \left(\frac{1}{T} - \frac{1}{T_0}\right)\right]$$

	High viscosity propellant paste	Fast burning liquid core
Inlet pressure:	24,82 MPa	0,086MPa
Inlet temperature	293,15K	293,15K
Density:	1510kg/m³	1640kg/m³
Thermal capacity:	2000J/(kg*K)	2000J/(kg*K)
Dynamic viscosity (Pa*s):	$\eta = e^{\left(\frac{2848,8}{T} + 2,606\right)} * \dot{\gamma}^{(0,205-1)}$	150
Thermal	0,294W/(m*K)	0,3W/(m*K)

Results: Results emphasize the relevance of the viscous heating and the shear thinning behavior of this rheologically complex fluid in the design process of the extrusion dies. Figure 3 illustrates the velocity profile and Figure 4 represents the thermal distribution under steady flow conditions.

conductivity:

Conclusions: The simulations shade light on the interaction between the power law index "n" and the viscous heating in the die design. The results obtained by finite elements simulations have been validated experimentally.

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