

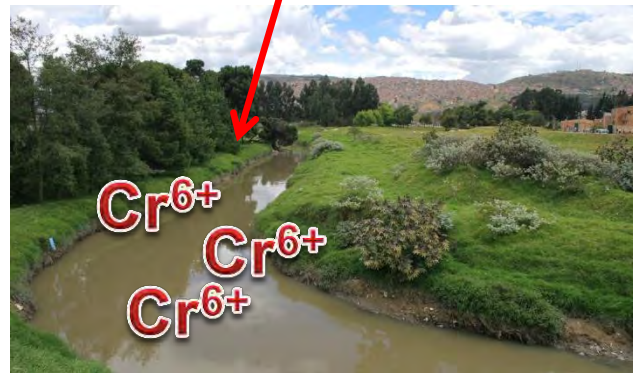
Presented at the 2011 COMSOL Conference in Boston

# Model of a Heavy Metal Adsorption System Using the S-Layer of *Bacillus sphaericus*

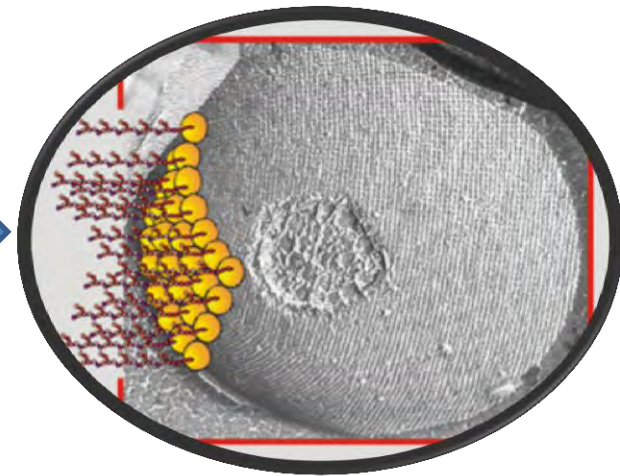
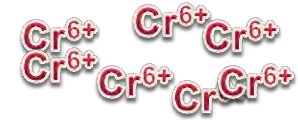
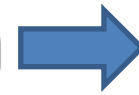
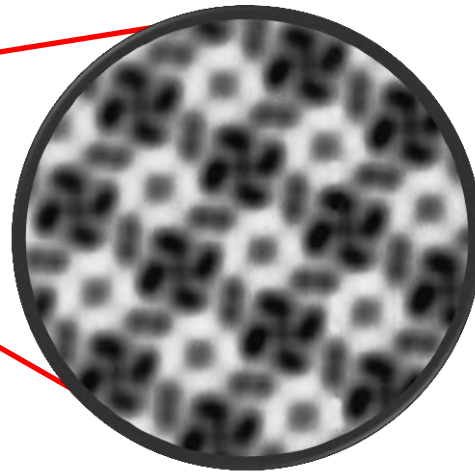
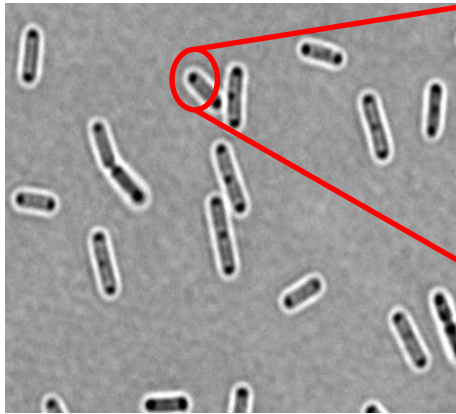
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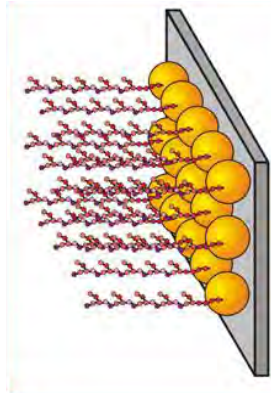
## Heavy metals and water



## *Bacillus sphaericus*



# Tunjuelito meets Bogotá



**Let's model this!**

$$\varepsilon_e \frac{\partial C_i}{\partial t} + \rho_p (1 - \varepsilon_e) \frac{\partial \bar{q}_i}{\partial x} + \varepsilon_e \frac{\partial (u \cdot C_i)}{\partial z} = \varepsilon_e (E + D_m) \frac{\partial^2 C_i}{\partial z^2}$$

$$\rho_p (1 - \varepsilon_e) \frac{\partial \bar{q}_i}{\partial t} = K_m \cdot a_p [C_i - C_i^*]$$

- Langmuir's Isotherm

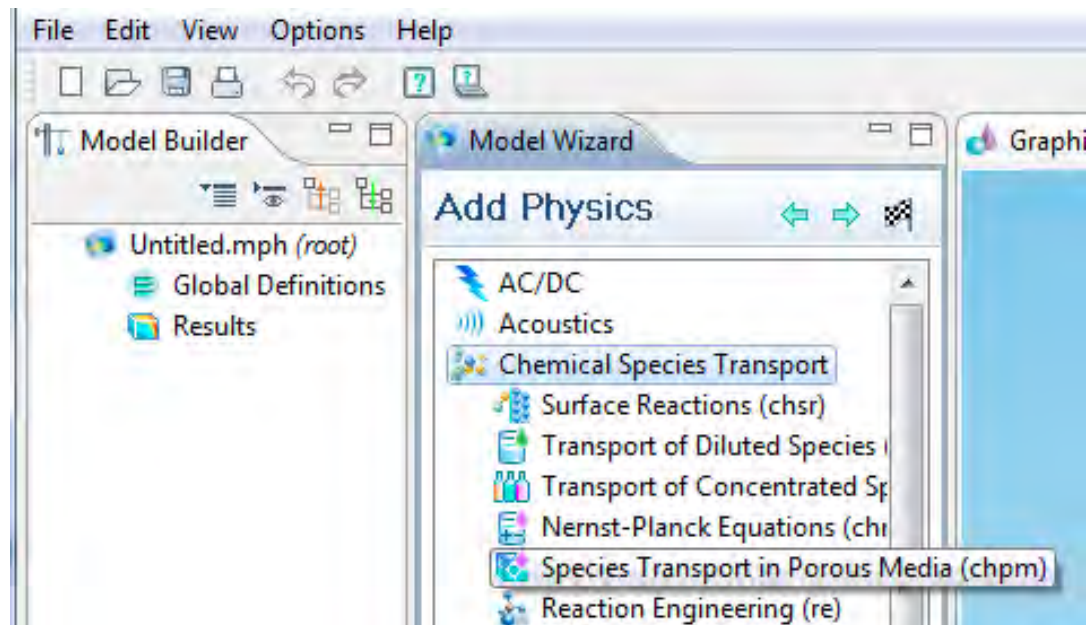
$$q_i = \frac{QC_i^*}{k + C_i^*}$$



## Use of COMSOL Multiphysics

- 2D
- Mass transfer module
- Chemical Species Transport / chpm

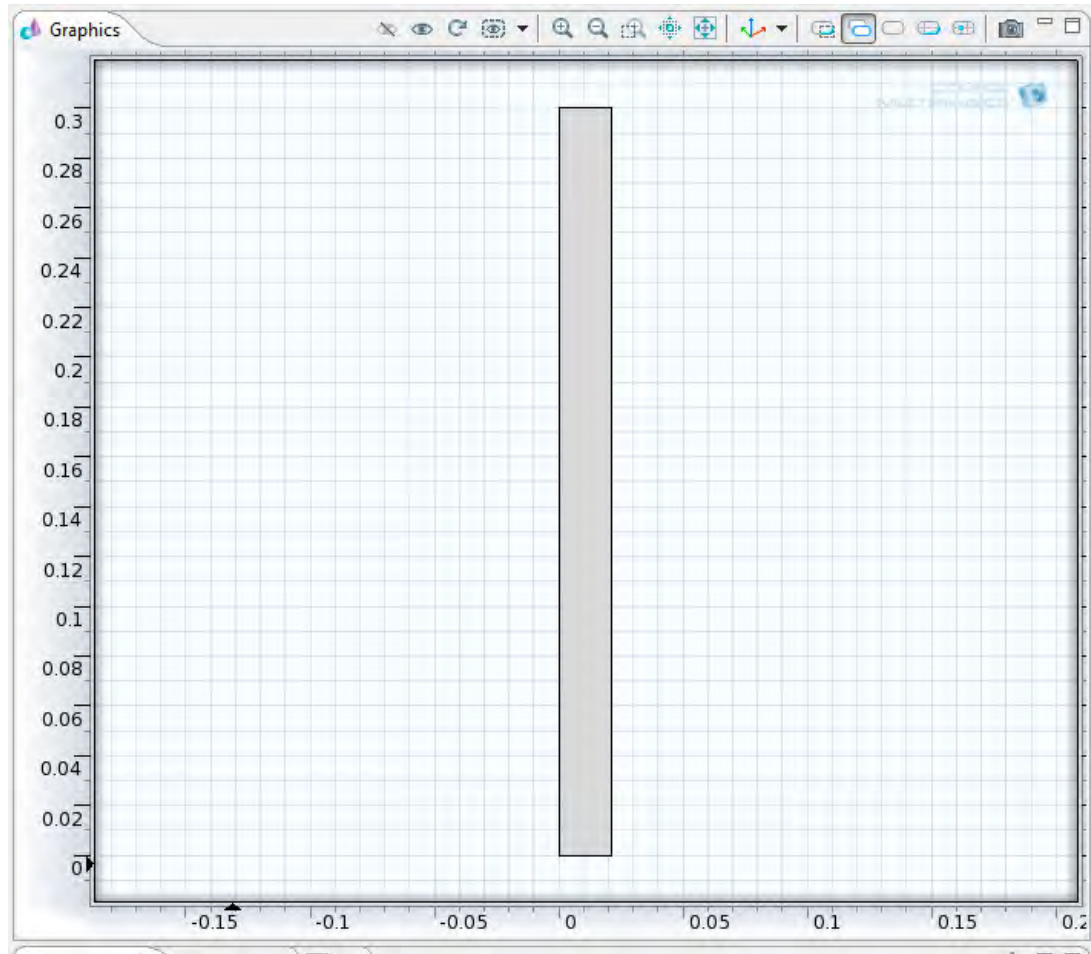
$$\delta \frac{\partial c_i}{\partial t} + \nabla \cdot (-D_i \nabla c_i) = R_i - \mathbf{u} \nabla \cdot c_i$$



## Global parameters

- Experimental:
  - Langmuir
  - Time for saturation
  - Density
  - Porosity
  - Initial concentrations
- Literature:
  - $D_m$
  - $E$
  - $K_m$

# Geometry





# Species transport in porous media

## Equation

Show equation assuming:

Study 1, Time Dependent

$$P_{1,j} \frac{\partial c_j}{\partial t} + P_{2,j} + \nabla \cdot \mathbf{\Gamma}_j + \mathbf{u} \cdot \nabla c_j = R_j + S_j$$

$$P_{1,j} = (\epsilon + \rho_b k_{p,j})$$

$$P_{2,j} = (c_j - c_{p,j} \rho_b) \frac{\partial \epsilon}{\partial t}, \quad \rho_b = \frac{\rho_b}{(1 - \epsilon)}$$

$$\mathbf{N}_j = \mathbf{\Gamma}_j + \mathbf{u} c_j = -(D_{D,j} + D_{e,j}) \nabla c_j + \mathbf{u} c_j$$

## Model Inputs

## Coordinate System Selection

## Porous Media

Porosity:

$\epsilon$  eps 1

Bulk density:

$\rho_b$  rho\*(1-eps) kg/m<sup>3</sup>

## Adsorption

Species c:

Langmuir

$$c_{p,j} = \frac{k_{L,j} c_{p,max,j} c_j}{1 + k_{L,j} c_j}, \quad k_{p,j} = \frac{\partial c_{p,j}}{\partial c_j} = \frac{k_{L,j} c_{p,max,j}}{(1 + k_{L,j} c_j)^2}$$

Langmuir constant:

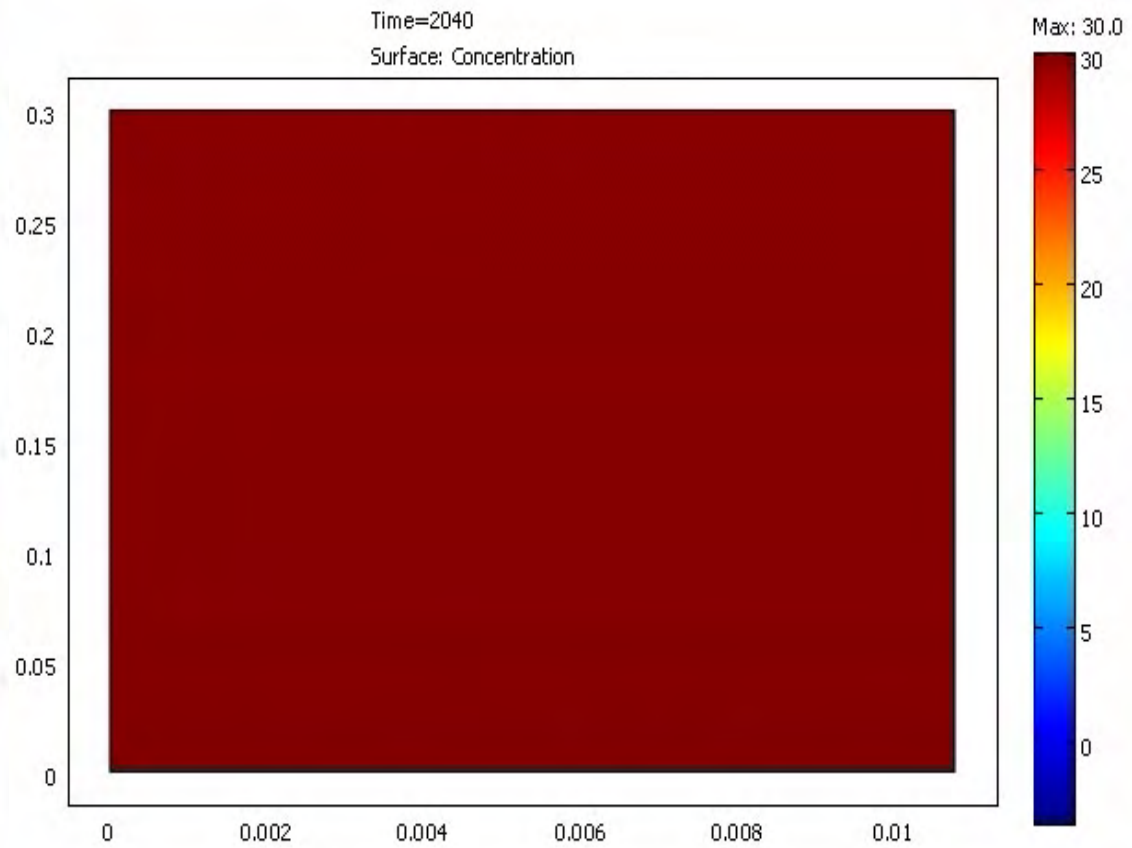
$k_{L,c}$  b m<sup>3</sup>/mol

Adsorption maximum:

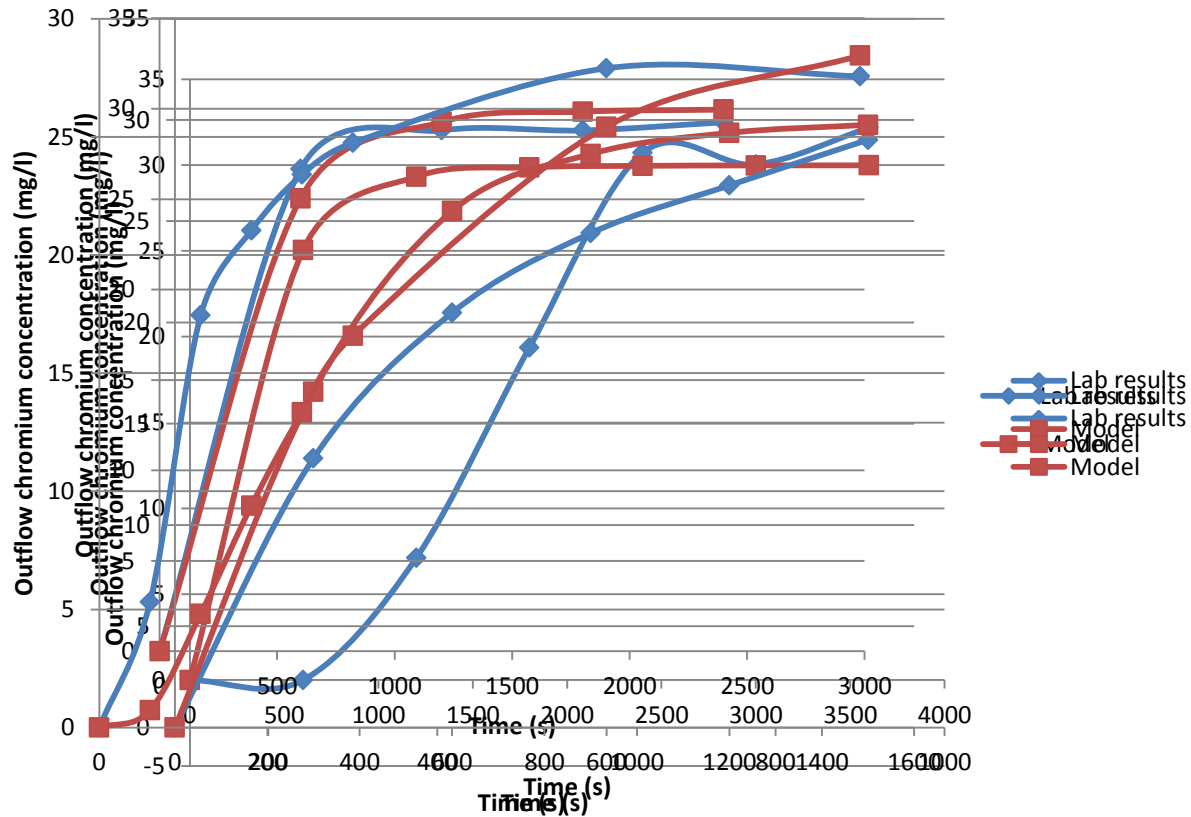
$c_{p,max,c}$  Q0\*S mol/kg

## Dispersion

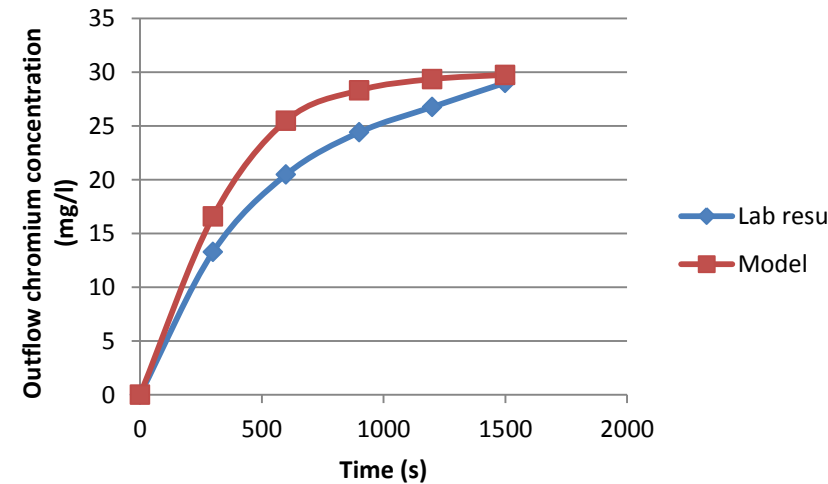
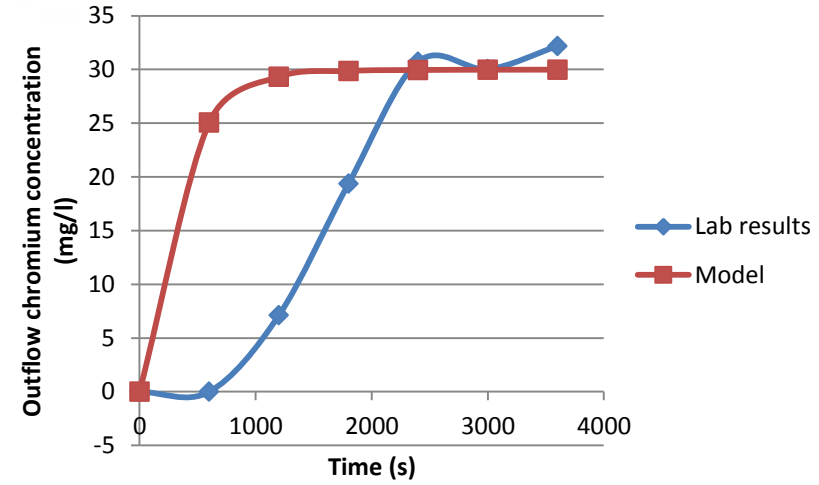
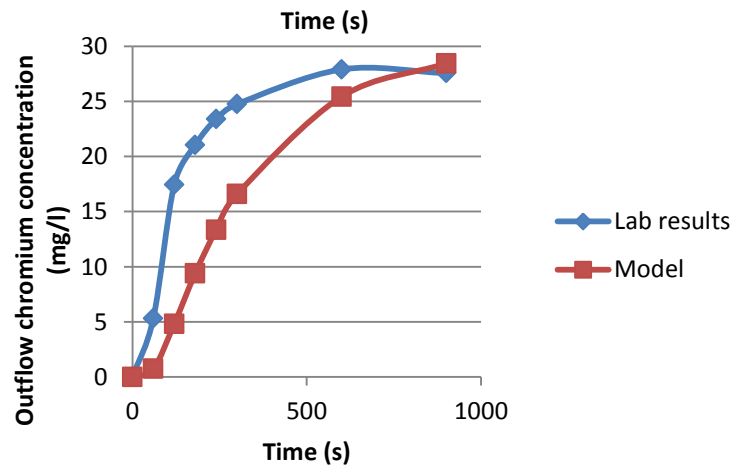
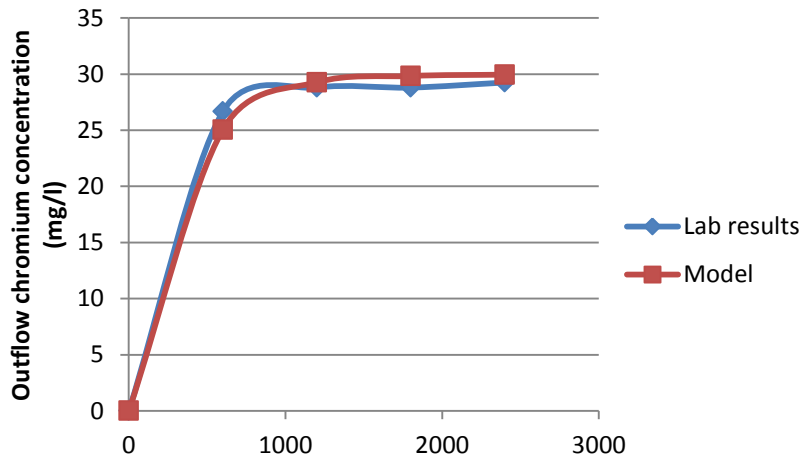
# Results



## Results II



## Results II



## Conclusions

- The model shows some really good preliminary results
- 1-D analysis is a good option
- Particle size has a greater effect than inflow speed
- Relationship between surface area and diffusivity coefficient ?
- Scale-up?



## Acknowledgements

- Civil and Environmental Engineering Department
- Urban and Regional Sustainability Group
- Chemical Engineering Department
- Biology Department
- Nathalia Flórez
- Andrea García
- Andrés Gonzalez

# THANK YOU!

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