

Flow and Mixing in the Liquid between Bubbles

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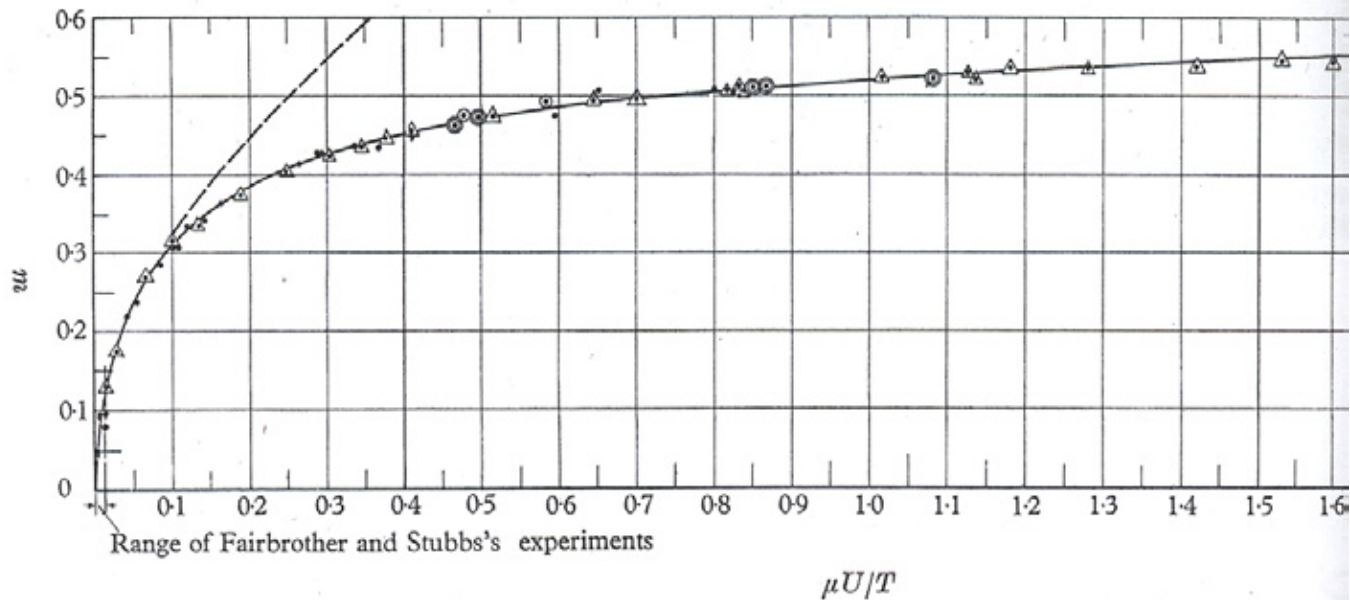
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G. I. Taylor, J. Fluid Mech. 10, 161 (1961)

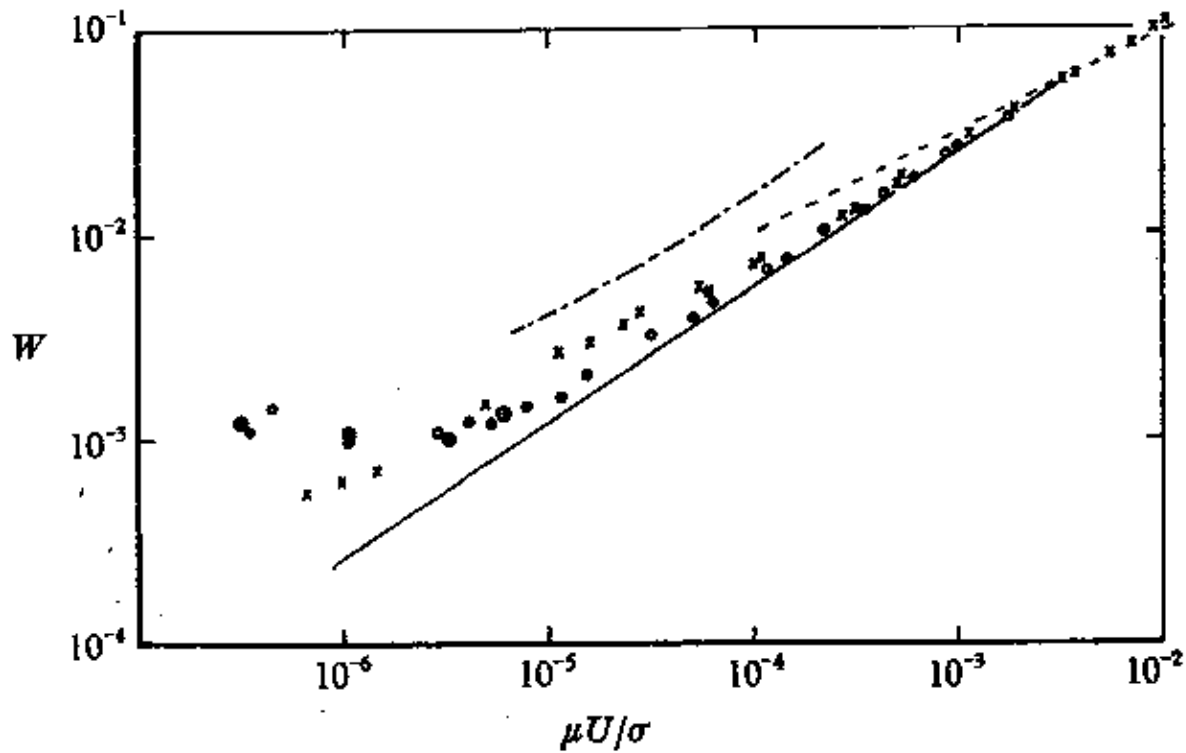
$$m = \frac{U_b - U}{U_b}, \quad m = 1.0(\eta U / \sigma)^{1/2} = 1.0 Ca^{1/2}$$

U = velocity of liquid, U_b = velocity of bubble

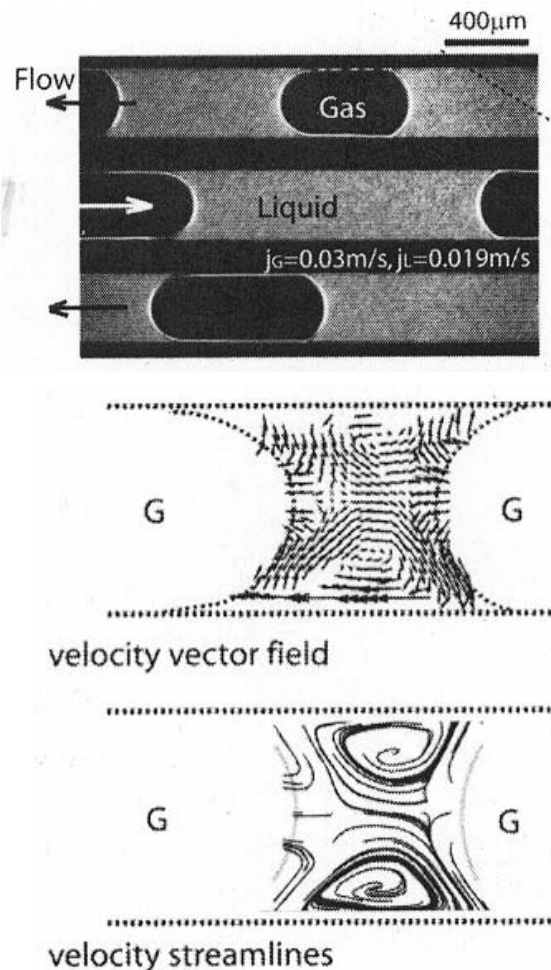
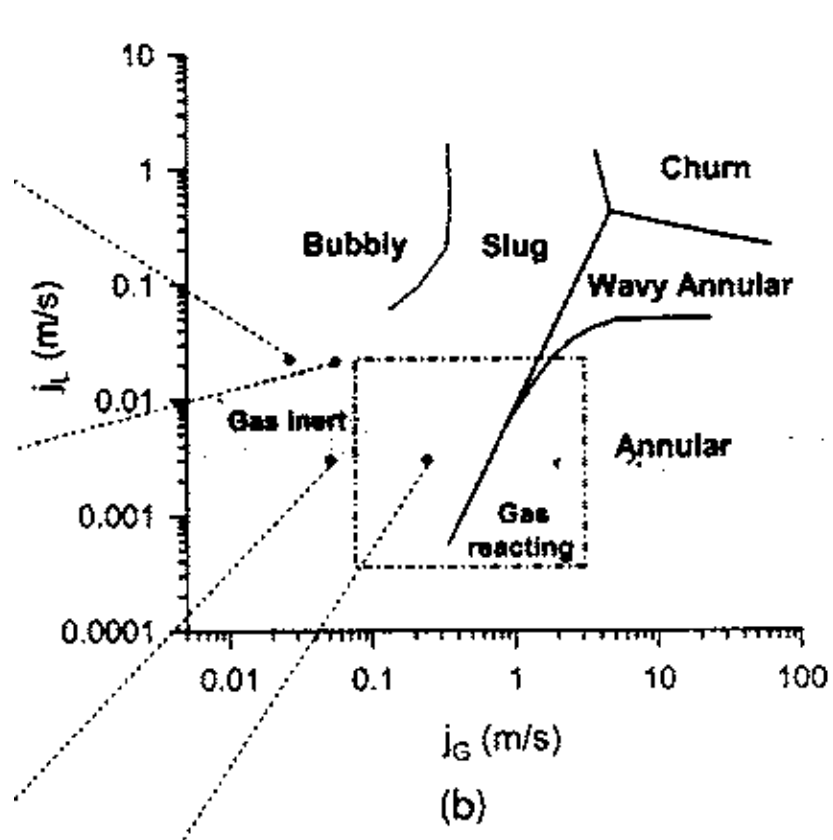


F. P. Bretherton, J. Fluid Mech. 10, 161 (1961)

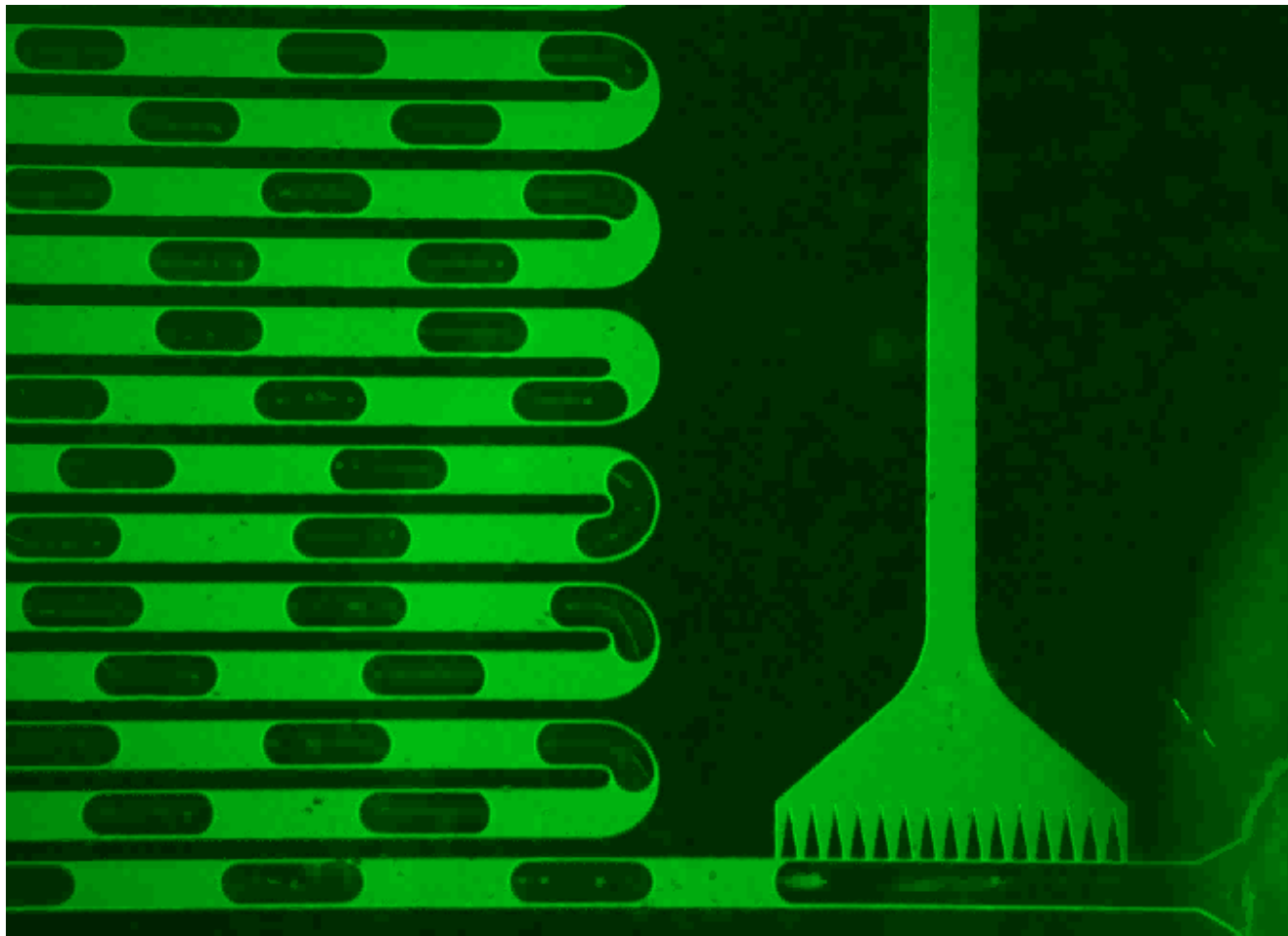
$$m = 1.29(3Ca)^{2/3}$$



Gunther, Khan, Thalmann, Trachsel, Klavs F. Jensen, Lab Chip, 4, 278 (2004)

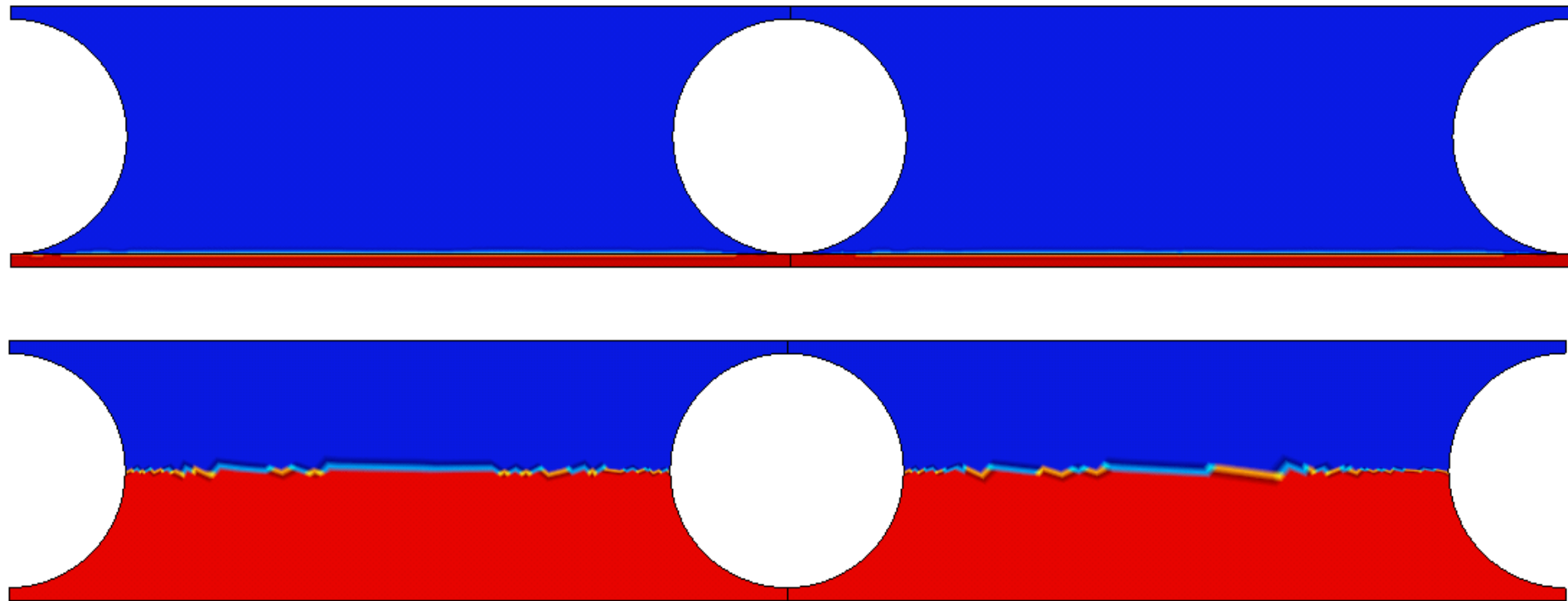


<http://www.rsc.org/suppdata/lc/b4/b403982c/>



Goal: quantify the mixing that occurs between the bubbles

- Case 1 – thin layer at bottom
- Case 2 – half and half



Flow – key assumption: assume a reasonable bubble shape, but don't solve for it; flow is steady

- Solve in a coordinate system moving with the bubble (velocity U_b)
- Non-dimensional equations

$$Re \mathbf{u} \cdot \nabla \mathbf{u} = -\nabla p + \nabla^2 \mathbf{u}, Re = 1$$

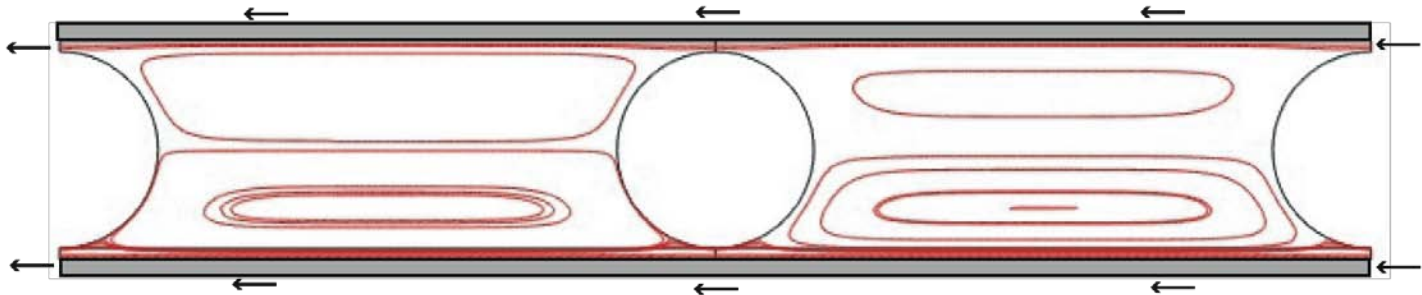
$\mathbf{u} = -1$ on solid boundary

zero stress on gas - liquid interface (perfect slip)

velocity specified at inlet to match these conditions

and have a specified flow rate

flow out the end



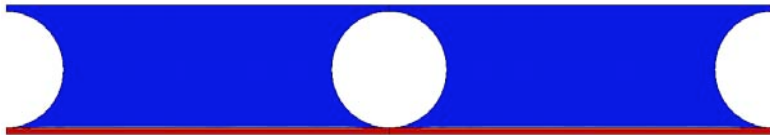
Unsteady Convection and Diffusion

- Concentration = 0 at one inlet, = 1 at other
- Zero flux on all bubble surfaces and wall
- Convective flux out
- Initial concentration for Case 1 and Case 2

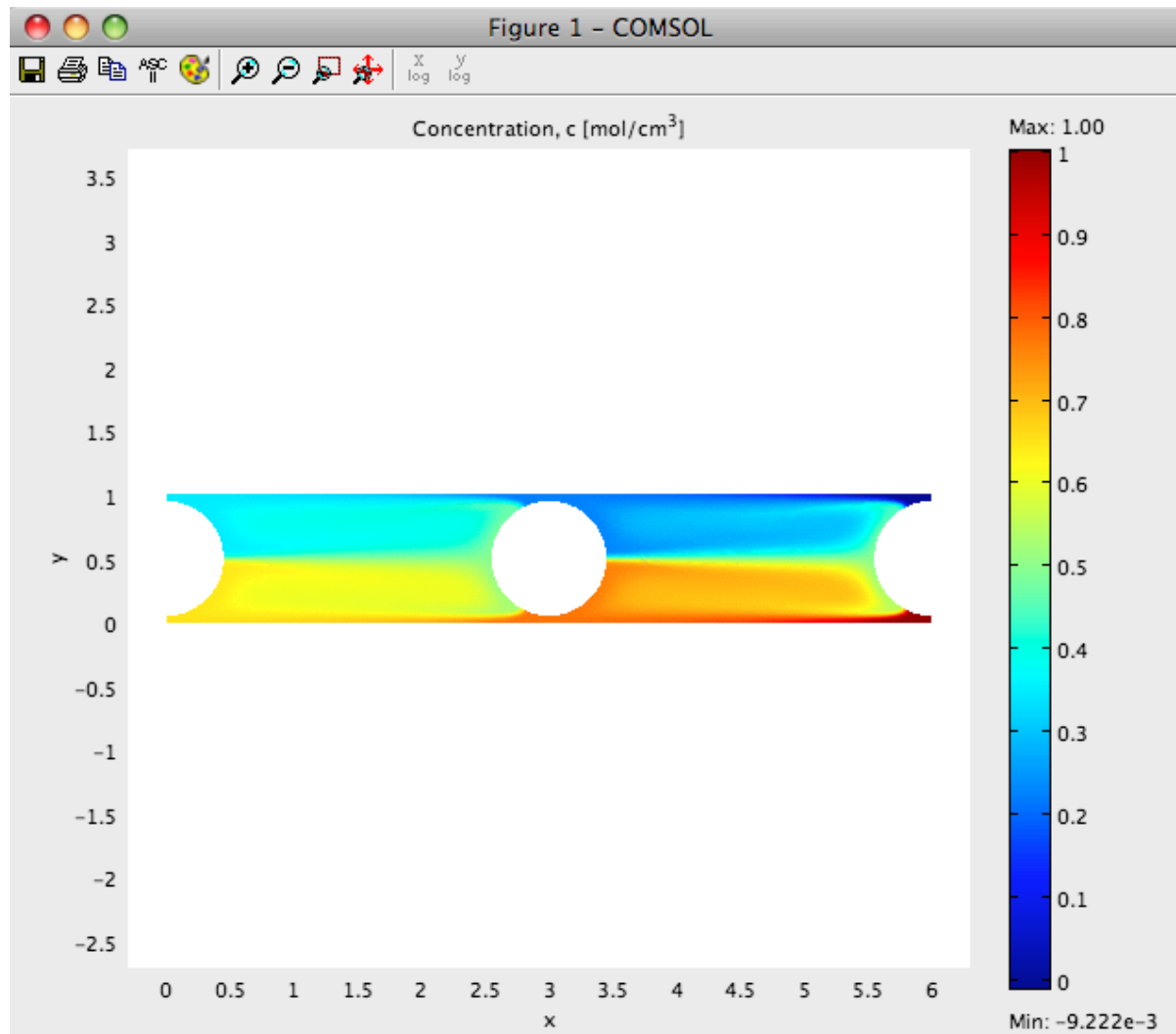
$$\frac{\partial c}{\partial t} + \mathbf{u} \cdot \nabla c = \frac{1}{Pe} \nabla^2 c$$

$$c_{avg} = \int_V c dV / V$$

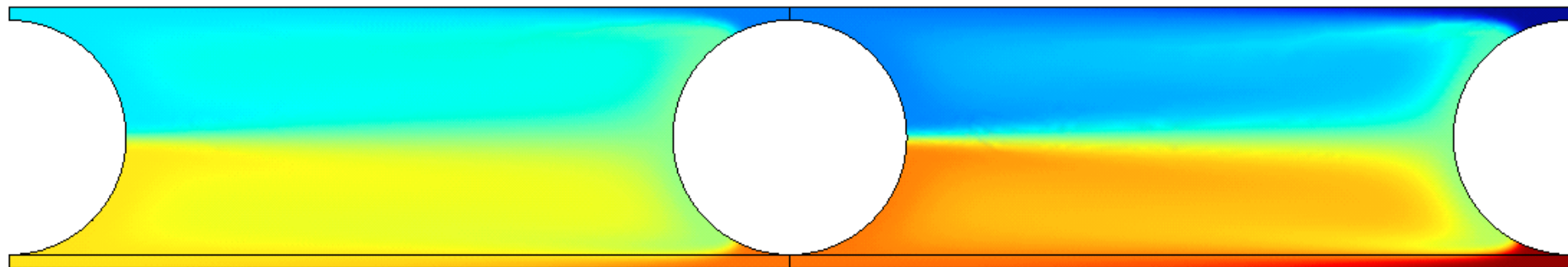
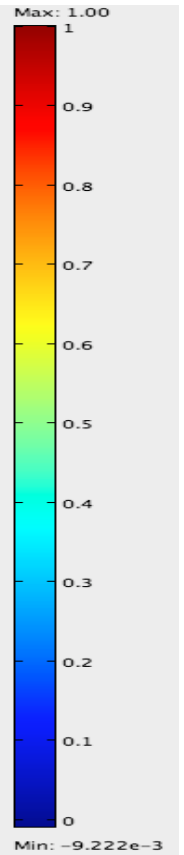
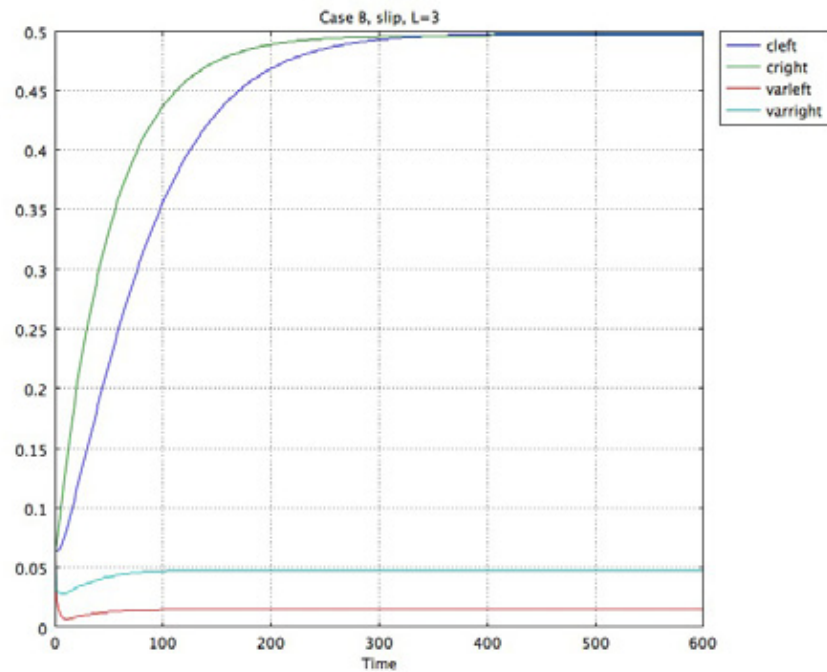
$$\text{variance} = \int_V (c - c_{avg})^2 dV / V$$



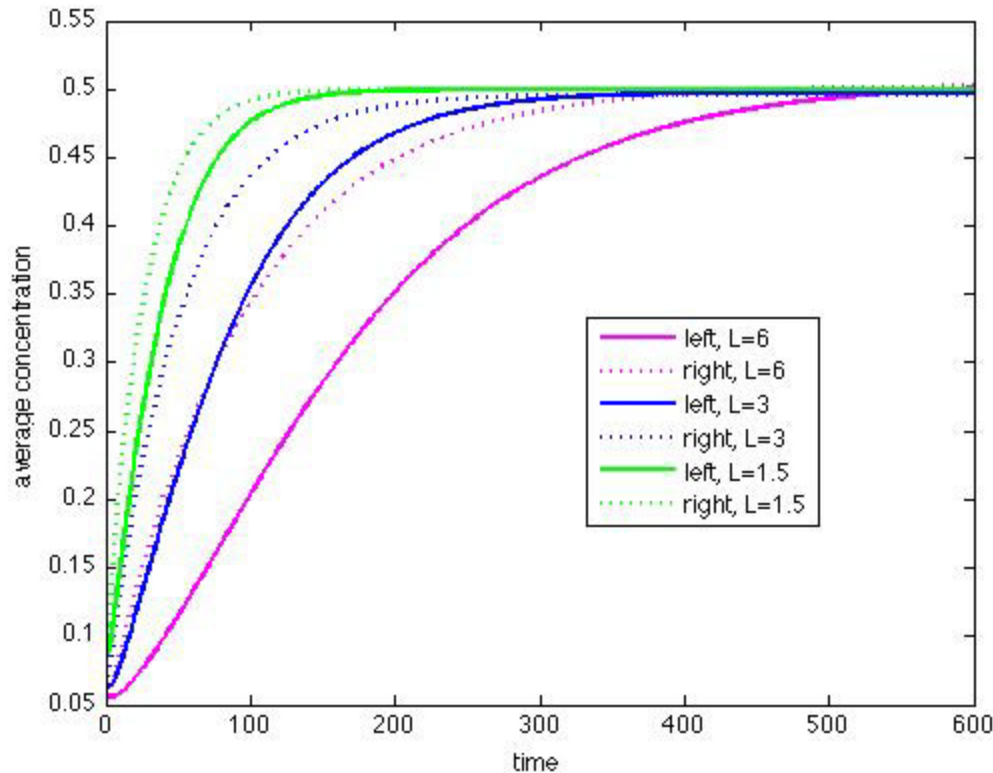
Concentration Development



Case 1 – B – base case



Effect of distance between bubbles



Variances

L = 6: 0.0049/.028

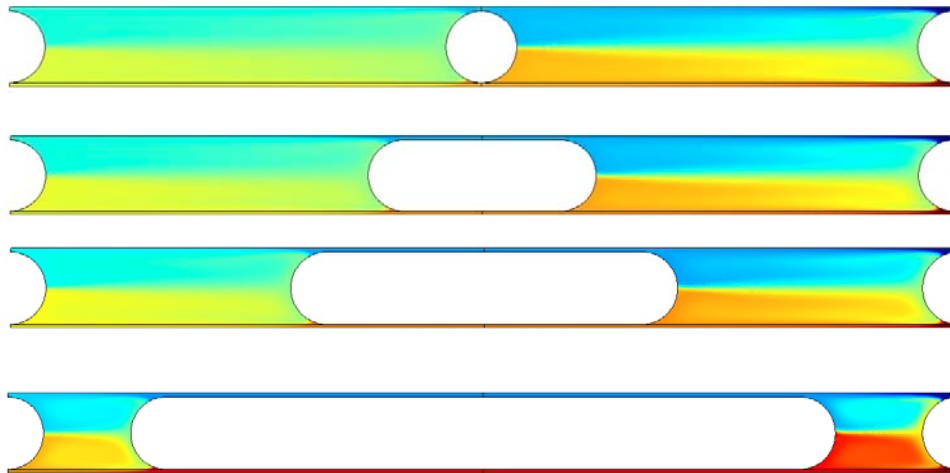
L = 3: 0.014/.048

L = 1.5: 0.055/.094

- For bubbles closer together, the variance is higher but it doesn't take as long to reach steady state

Effect of elongated bubbles

- Little effect on the approach to steady state but the variance increases as the length of the bubble increases



Bubble Length –

Left Variance/Right Variance

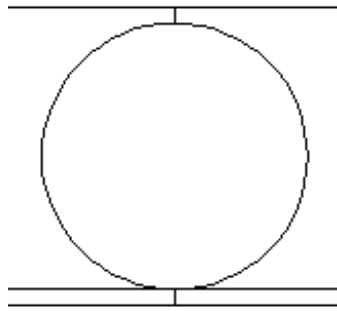
1 - .0049/.028

2 - .0073/.032

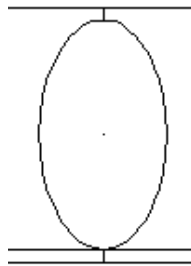
4 - .012/.039

6 - .043/.071

Effect of bubble shape



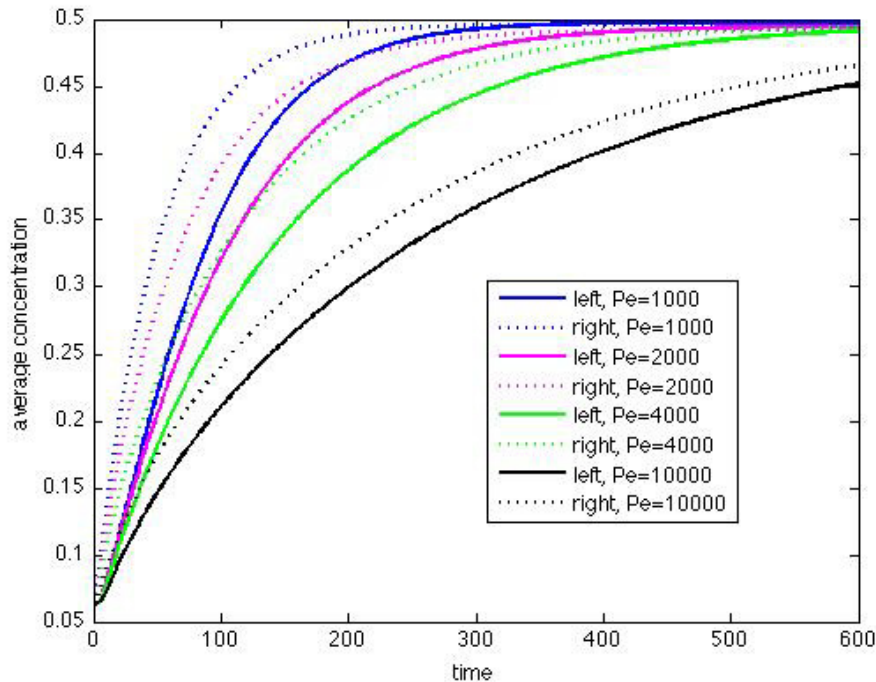
$$\text{Variance} = 0.014/0.048$$



$$\text{Variance} = 0.011/0.041$$

Shape makes little difference.

Effect of Peclet number



Peclet No. - Variance

1000 - .014/.048

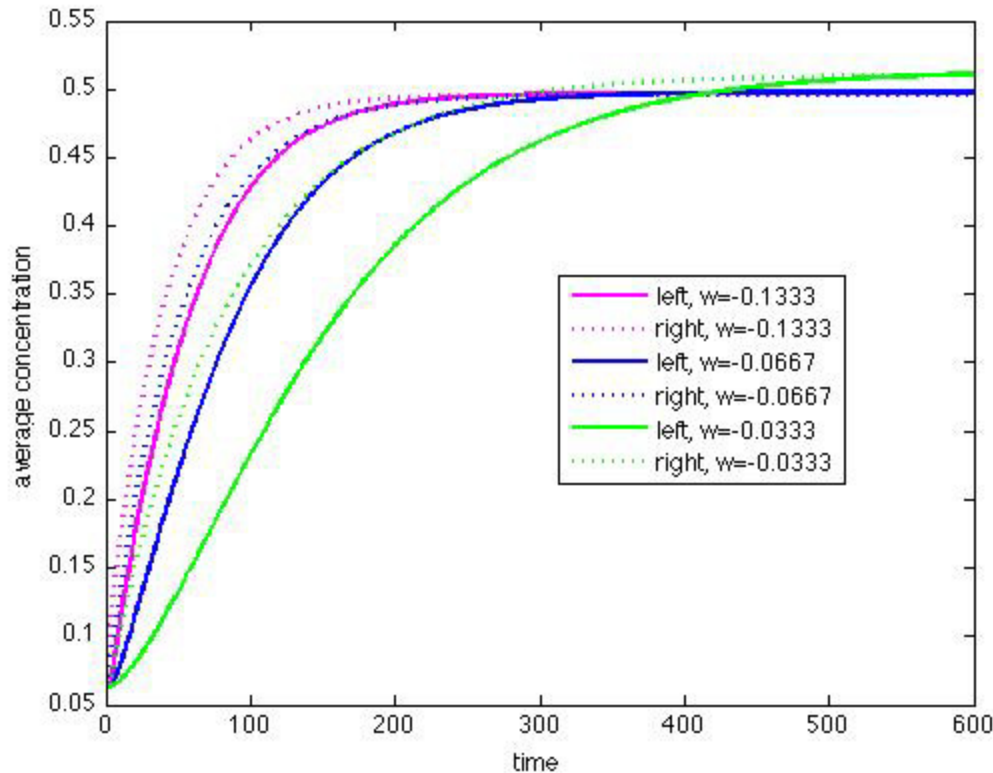
2000 - .024/.058

4000 - .034/.063

10000 - .041/.063

- As the Peclet number increases, it takes longer to reach steady state and the steady variance is larger

Effect of leakage rate



Leakage Rate/Variance

-.13 - .046/.077

-.07 - .014/.048

-.03 - .0026/.021

-.01 - 4e-4/.01

- As the leakage rate increases, the time to steady state decreases, and the variance increases

Effect of gap thickness

- The smallest variances are for smaller gaps and smaller leakage rates
- A leakage rate of -0.01 is an average of what is predicted by Taylor (-0.012) and Bretherton (-0.0072) for a Capillary number of 0.00014 (air/water)

Leakage rate = -0.0667

Gap thickness/Variance

0.05 - .014/.048

0.03 - 4e-4/.01

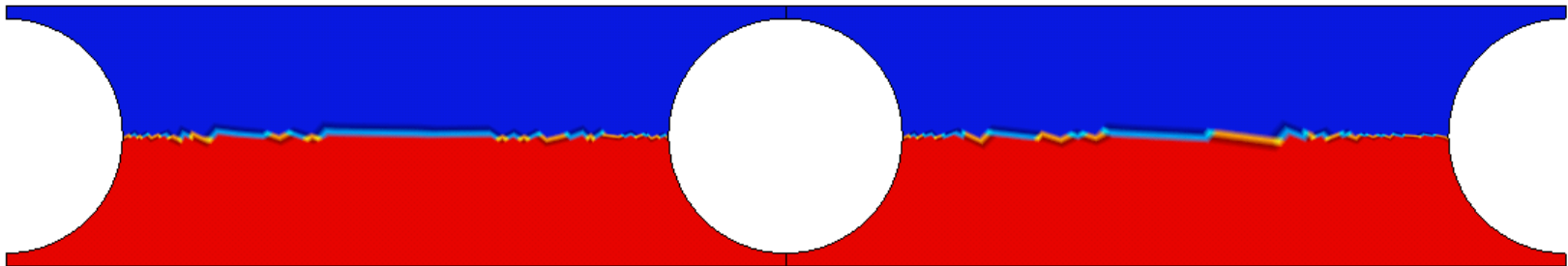
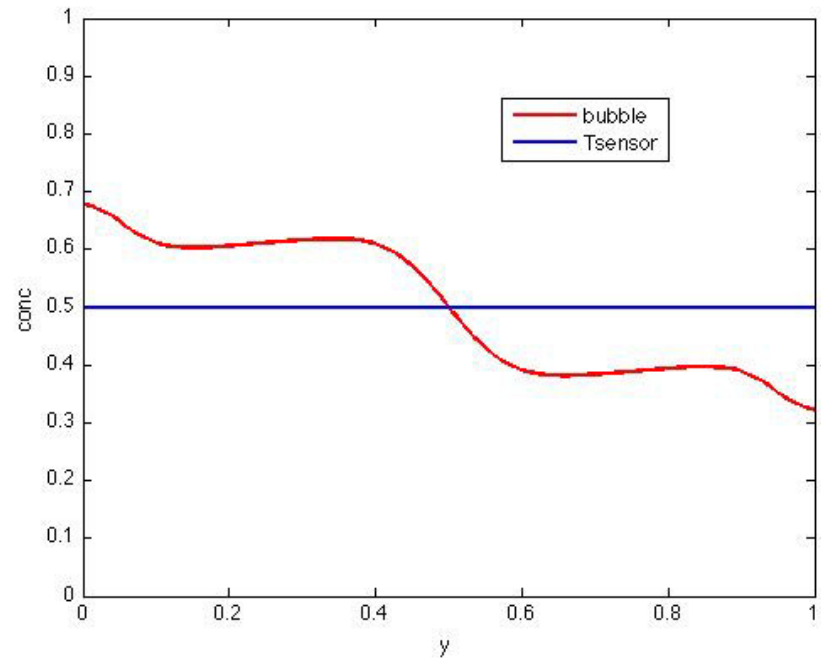
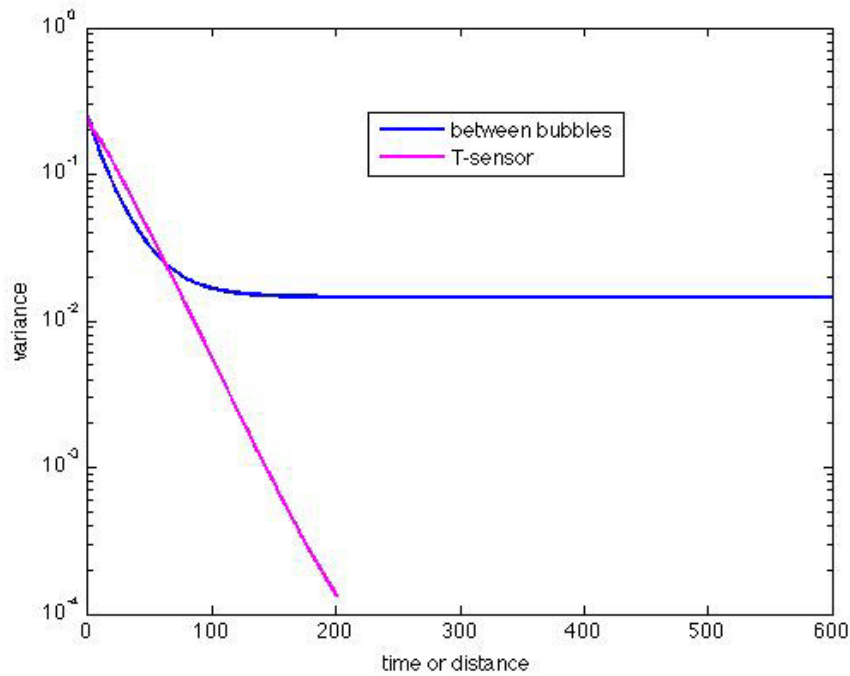
Leakage rate = -0.01

Gap thickness/Variance

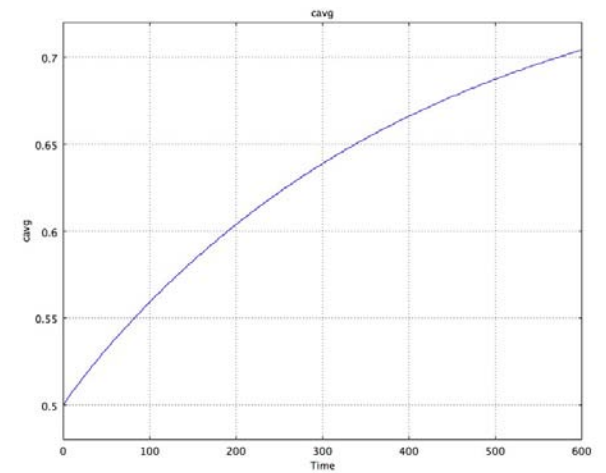
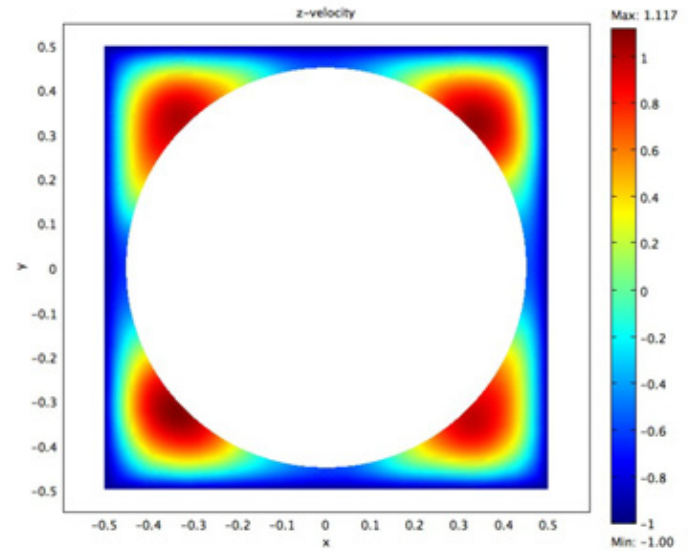
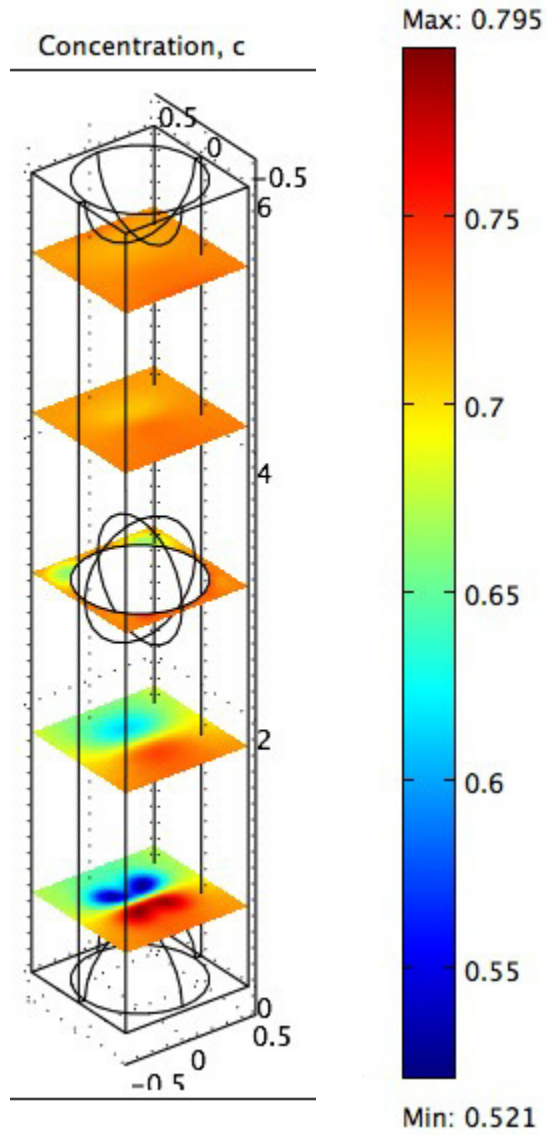
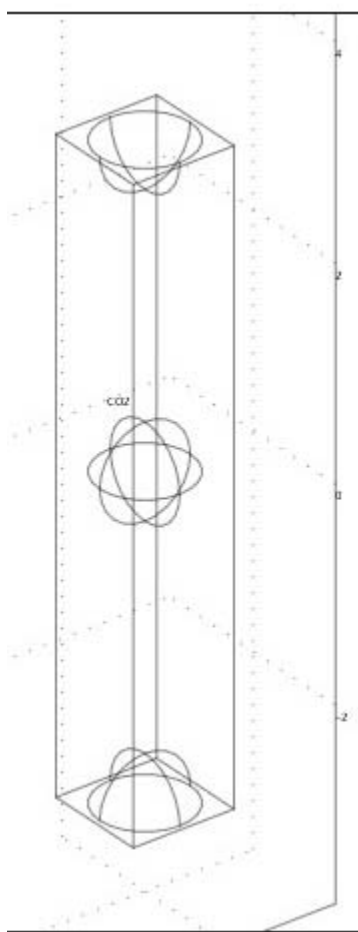
0.05 - .0044/.027

0.03 - 3e-4/.0043

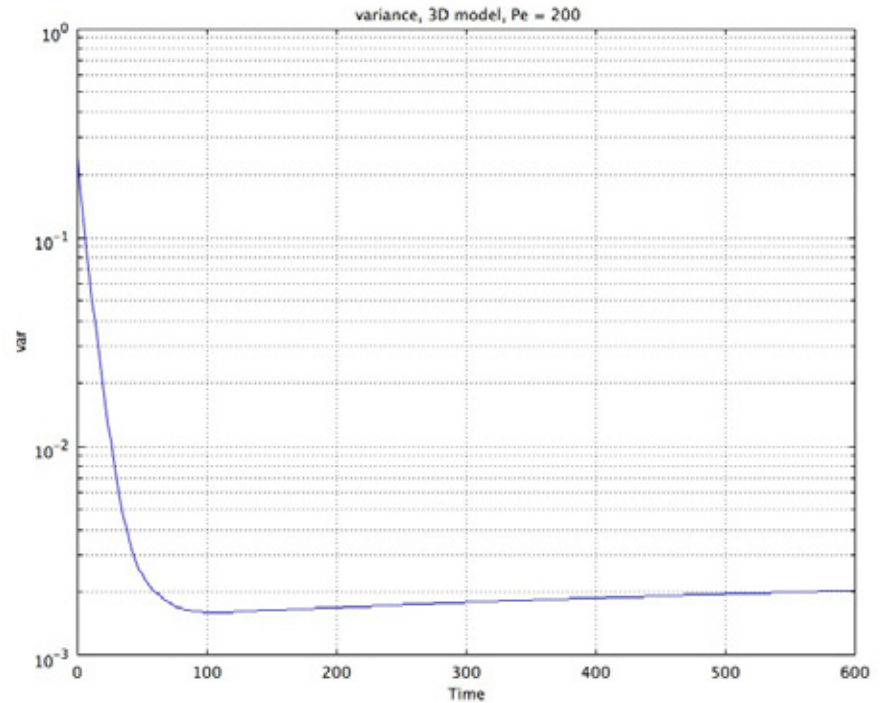
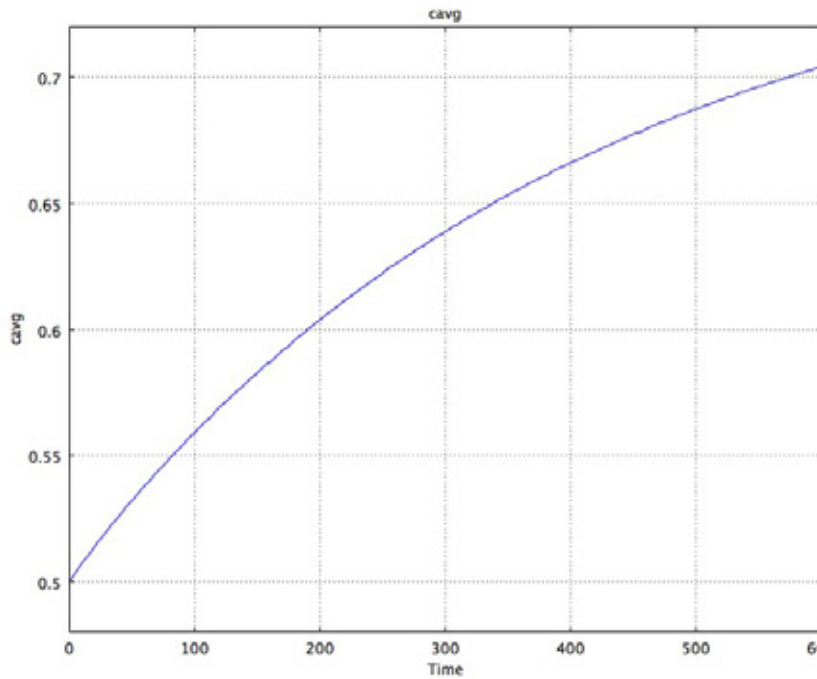
Results for Case 2; comparison with T-sensor



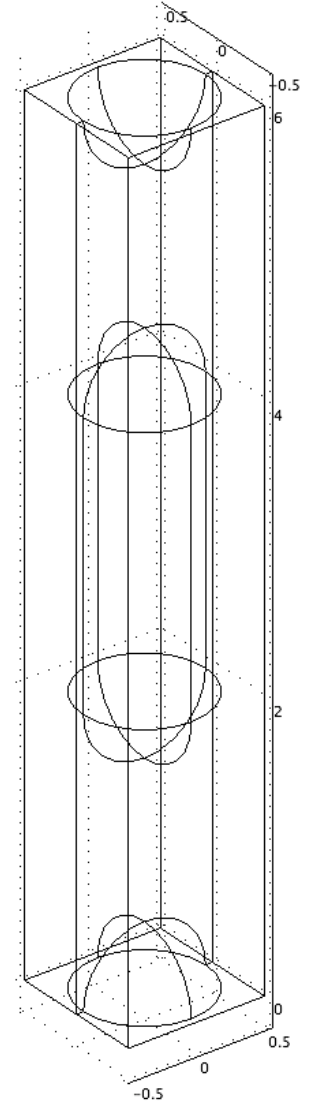
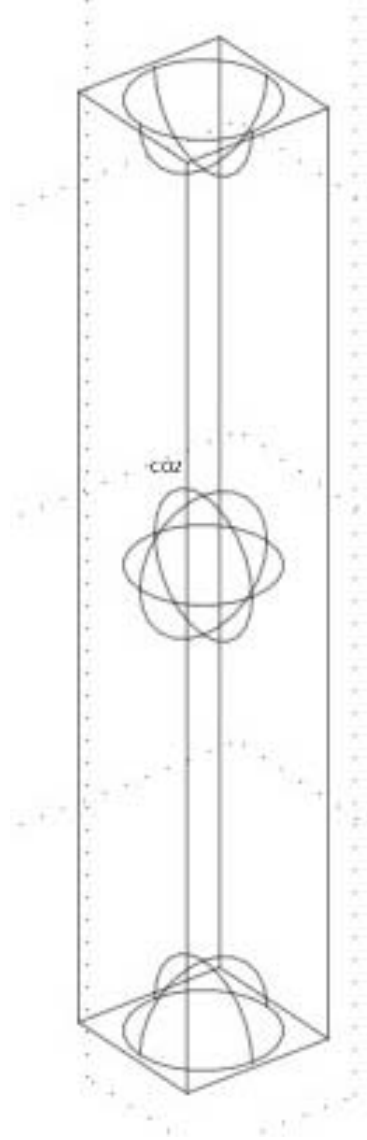
3D results



Cavg and variance in 3D

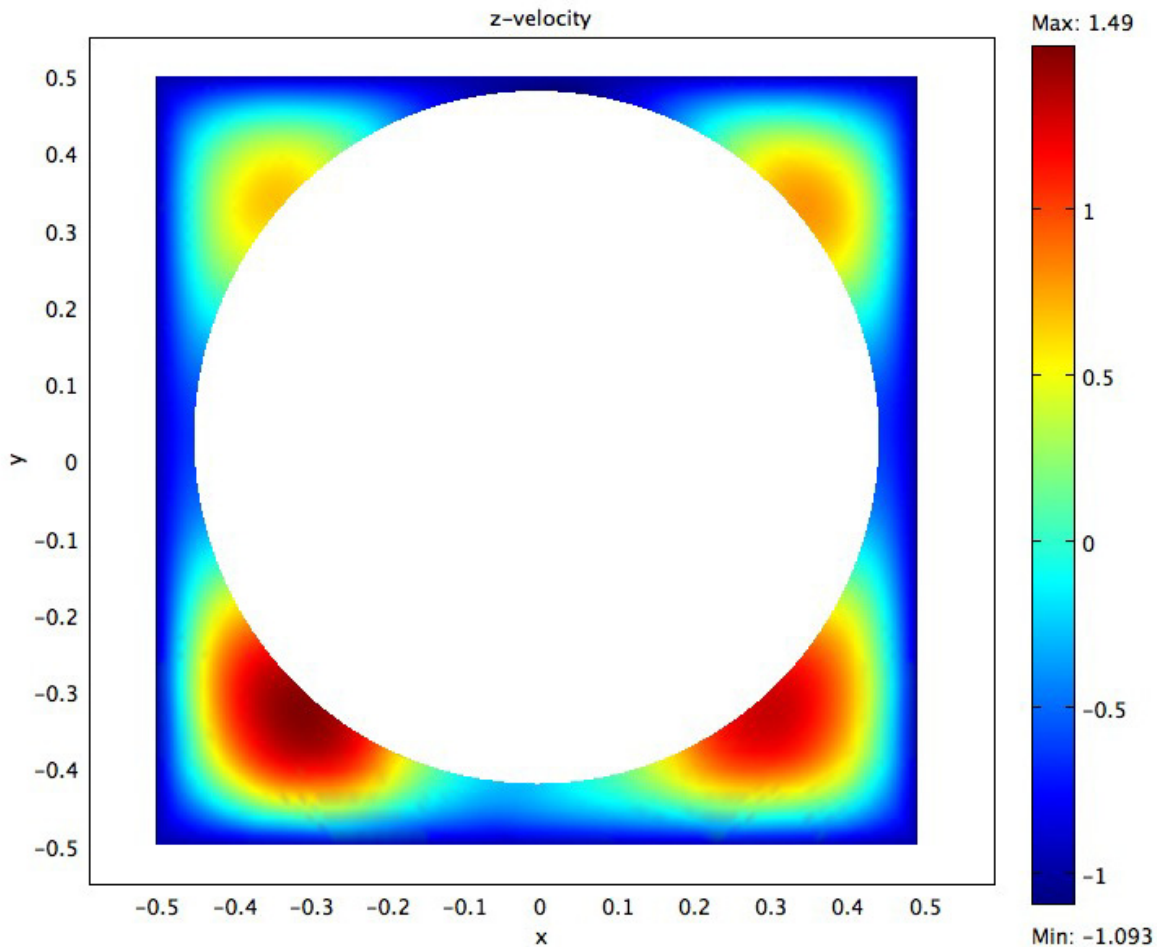


Effect of longer
bubble in 3D –
same as in 2D –
less mixing



- Variance – 0.002 0.019

Effect of bubble not centered



- Variance
- Centered - 0.002
- Offset - 0.0014
- improved mixing

Conclusions

- The variance always approaches an asymptotic value.
- While the geometry is assumed, the qualitative results are independent of the geometry.
- Better mixing is achieved by:
 - Bubbles further apart
 - Spherical bubbles, not elongated ones
 - Low leakage rates
 - Small gap thicknesses